



TRNSYS SIMULATION OF SOLAR ENERGY SUPPLY TO A MILK PROCESSING PLANT

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CONTEXT OF THE PRESENT STUDY



Saving water and energy for resource
efficient food processing



- ✓ Integration of solar heat into dairy industry processes will be demonstrated by **IRTA**
- ✓ The research work associated with the solar system design and sizing was developed by **IREC**
- ✓ **Pilot facility:** Combination of experimental solar system + experimental milk treatment system



OBJECTIVES OF THE STUDY

Challenges

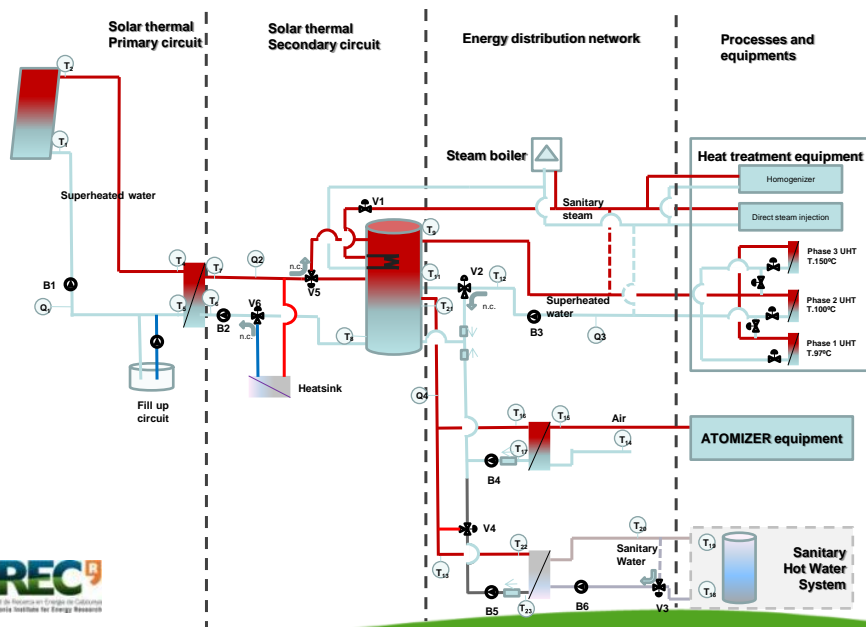
- ✓ To optimize the system configuration in order to increase solar thermal contribution (or solar fraction)
- ✓ To show that it is possible to achieve with conventional direct streamed Sidney vacuum tube solar collectors a middle temperature range of 150°C for experimental UHT applications in a southern European country

Outputs from TRNSYS simulations

- ✓ Size of storage tank and solar field
- ✓ Outcome of possible system configurations to define optimal installation and control schemes
- ✓ Assessment of duration of periods with 100% solar operation to feed-in the storage tank and UHT process

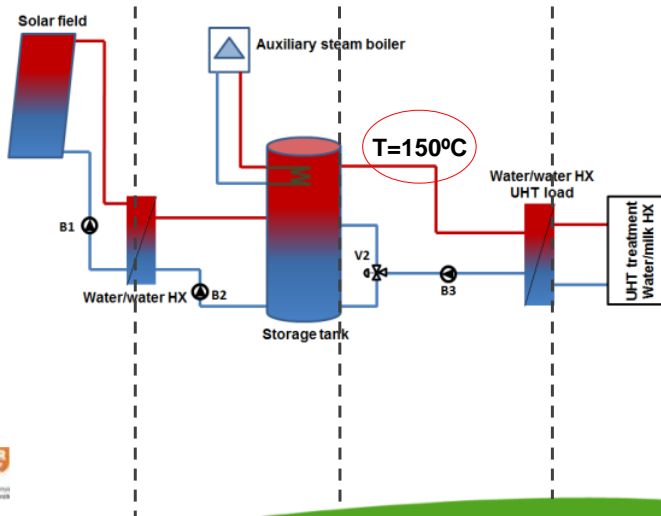


SCHEME OF THE PILOT FACILITY



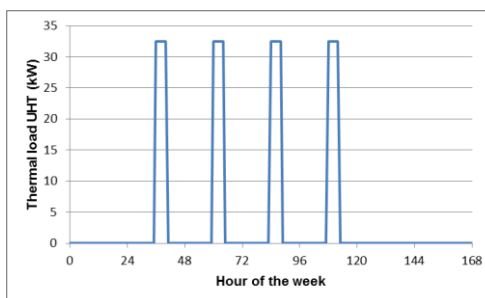
TRNSYS SOLAR THERMAL SYSTEM MODEL

Solar thermal Primary circuit Solar thermal Secondary circuit Energy distribution network Processes and equipments



TRNSYS SOLAR THERMAL SYSTEM MODEL

Working fluid	Superheated water at 150°C Hydraulic system pressure 8.5 bar
Solar field	Direct-flow evacuated tube solar collector Model: Buderus - LOGASOL SKR12.1 Collector absorber area = 2.57m ² Number of collectors in series = 5 Total number of collectors = 40; 30; 20
Storage tank	Volume = 5 000 L, 4 000 L, 2 500 L; 1 000 L Hydraulic system pressure 8.5 bar

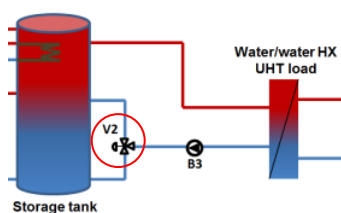


RESULTS FROM PARAMETRIC ANALYSIS

- (1) INTRODUCTION OF STRATIFICATION VALVE V2
- (2) NUMBER OF SOLAR COLLECTORS AND TANK SIZE
- (3) INTRODUCTION OF STRATIFICATION VALVE V5



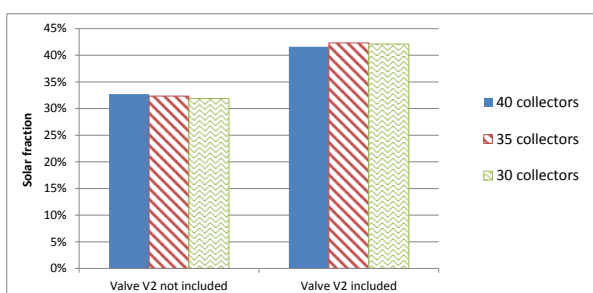
RESULTS FROM PARAMETRIC ANALYSIS INTRODUCTION OF STRATIFICATION VALVE V2



✓ Fixed tank size (5 000 L)

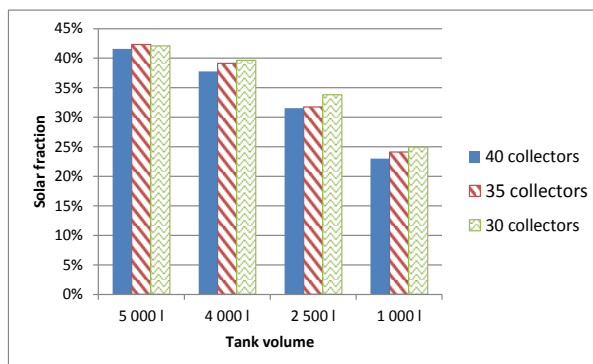
$$SF = \frac{Q_{UHT} - Q_{boiler}}{Q_{UHT}}$$

- ✓ Better stratification in the tank
- ✓ Lower boiler usage
- ✓ Higher solar energy

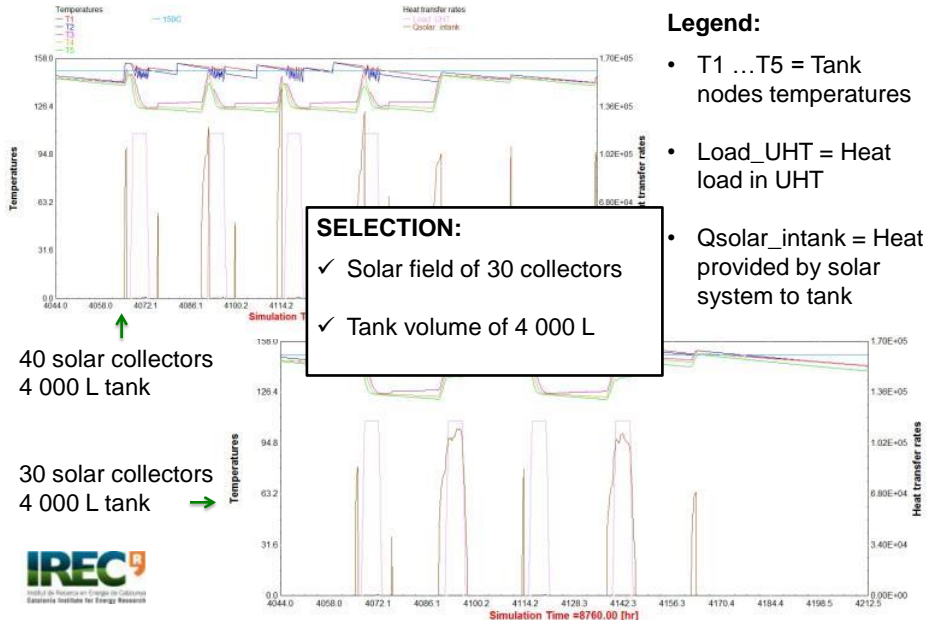


RESULTS FROM PARAMETRIC ANALYSIS NUMBER OF SOLAR COLLECTORS AND TANK SIZE

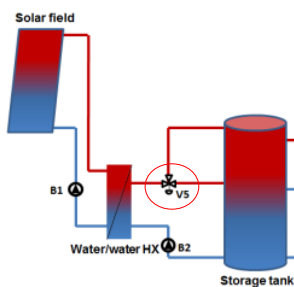
- ✓ The larger the tank, the larger the solar fraction obtained.
- ✓ The configuration with 30 collectors gives a larger solar fraction.



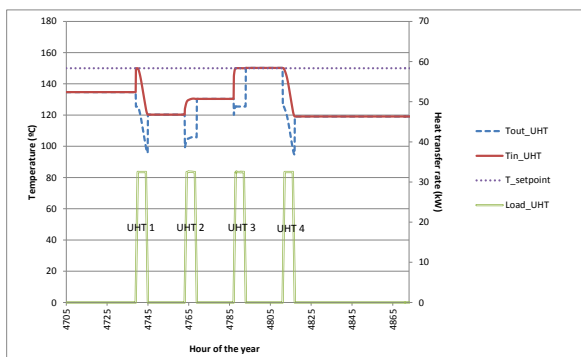
RESULTS - TANK TEMPERATURES AND SOLAR ENERGY



RESULTS FROM PARAMETRIC ANALYSIS INTRODUCTION OF STRATIFICATION VALVE V5



Valve V5	Time when $T_{in_UHT} \geq 150^{\circ}C$	Nr. of days when complete UHT process experiment is exclusively supplied by solar energy
	Hours / year	Days / year
Not included	3.50	0
Included	56.88	4



CONCLUSIONS

- ✓ Solar fraction is enhanced by installing 30 collectors in front of 35 or 40 collectors in the present system
- ✓ Introduction of stratification valve V2 in the cold return from UHT process leads to an increase of the annual solar fraction of 10%
- ✓ Introduction of stratification valves V2 and V5 → 100% solar fraction is accomplished during few days per year with continuous 150°C water supply to the experimental milk treatment process
- ✓ Size of the facility to reach a maximum annual solar fraction of **39.6%** assessed using TRNSYS:
 - Solar field: 77 m², 30 ETC, 2.57 m²/u (absorber area)
 - Storage tank: 4 000 L





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